

**K BEŞ GAYRİMENKUL
DANIŞMANLIK**
İnş. Taah. Tur. San. Ve Dış Tic. Ltd. Şti.



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EEIG
EUROPEAN ECONOMIC CHAMBER OF TRADE,
COMMERCE AND INDUSTRY**

İSTANBUL - AFYON - TÜRKİYE

Clinker section :

1) the feeding size of clinker retarder section :

2) gypsum : type, feeding size, moisture (mixed material section : refers to the other material is added in cement grinding)

3)slag : feeding size, moisture

4) coal ash : powder id our of the electric dust collector, or heap yard block (particle size,moisture)

Note: other kinds of composite materials (such as limestone, etc.), according to the country's resources.

fuel material (slag or other containing water material need baking, this be provided)

5) industrial analysis of coal (volatile, ash content, fixed carbon, calorific value etc.),

particle size, moisture into the factory.

chemical analysis of coal ash

Note:other fuel,it need to provide the type (such as oil, gas, petroleum coke), the composition,calorific value, particle size, moisture, etc.

6) packing section :

bag type : bag weight, need the automatic loading machine or not ?

Bulk Type : library side in bulk, or in bulk at the bottom ?

other built factory conditions :

water : water, water quality, water quantity

electrical : electricity power grid voltage (11 kv or other), frequency (50hz or 60hz)

ichnography, landform geomorphological, geology (design should be according to

geological exploration report) customer need supply the information for the grinding station as follows;

1. elevation, weather etc.

2 Basis of design

2.1 Design capacit ____ ton clinker per day

2.2 Plant site condition:

2.2.1 altitude of the site above sea-level:

2.2.2 Temperature

Annual average temperature/year: ____ C

Average temperature in summer: ____ C

Max. temperature: ____ C

Min. temperature: ____ C

2.2.3 Rainfall

Max. rainfall for calendar year: ____ mm

Max. rainfall for calendar year: ____ mm

Max. rainfall for calendar year: ____ mm

2.2.4 Humidity

Annual average relative humidity: ____ %

Relative humidity for Max. hot monthly mean: _____%

2.2.5 Wind speed

Annual average wind speed: _____

10 minute average max. wind speed: _____ m/s

2.2.6 Sun light Average sun light time for calendar year: _____ h/day

2.2.7 Max. freezing soil depth: _____ mm

2.2.8 Min. freezing soil depth: _____ mm

2.2.9 Annual average thunder days: _____ days

2.2.10 Main wind direction

Main wind direction for calendar year summer: _____

Main wind direction for annual average season: _____

2.2.11 Information about the earthquake, thunder and hailstone



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K BEŞ GAYRİMENKUL DANIŞMANLIK İNŞ.TAAH.TUR.SAN.VE DİŞ TİC.LTD.ŞTİ.

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İrtibat: Dumankaya Vizeyon E-5 Karayolu İstiklal Cad. No:57 Kartal – İstanbul/2.Dumlupınar Cad. Koçoğlu İş Merkezi Kat:3/7 AFYON

MACHINERY AND BRANDS USED IN ELECTRICAL UNITS

Reducer	– YILMAZ REDUKTOR
Electric Motors	– GAMAK (from 0,06 to 1000KW.EU engines will be used for the engines higher than 1000KW)
Electrical Materials	– OMRON
Contactors	– OMRON, SIEMENS, TELEMKANİK
Automation	– OMRON (Plc)
Sensors	– OMRON
Inverter	– OMRON
Communication	– OMRON
Encoders	– OMRON
Servo System	– OMRON
Motor Control	– OMRON
Capacitor Load Circuit	– MADE IN TURKEY
Load Relays	– OMRON
Cables	– OF TSE
Thermal Camera Sensitive To Heat	– OMRON
Heat Meters	– OMRON
Silo Level Indicators	– OMRON
Weighing Cells	– ESIT ELEKTRONİK
Load Cell	– ESIT ELEKTRONİK



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1200 t/d Cement Clinker Production Line

Technical Plan

(Adopt new model five-stage cyclone pre-heater kiln)

İSTANBUL-AFYON/TÜRKİYE

The Product List of 1200TPD Cement

NO	Name	Q'TY
I	crushing	
1	vibrating feeder	1
2	jaw crusher	1
3	belt conveyor	1
4	compound crusher	1
5	belt conveyor	1
6	Dust Collection	1
7	bucket elevator	1
8	de-iron separator	1
9	glass fiber dust collector	1
II	Drying	
1	tooth roller crusher	1
2	bUcket elevator	1
3	coal injection machine	1
4	drier	1
5	bUcket elevator	1
6	belt conveyor	1
7	Dust Collection	1
III	Raw material grinding	
1	automatic batching system	1
2	ball mill	3
3	electric dust collection	1
4	bUcket elevator	1
5	high-effect power concentrator	1
6	draughtfan	1
7	bucket elevator	1
8	belt conveyor	1
9	squama board conveyor glass fiber dust collector	1
10	hydranlic double roller crusher	1
11		2
IV	clinker	
1	feeder	3
2	screw conveyor	1
3	bucket elevator	1
4	screw conveyor	1
5	double-roller blender	1
6	automatic pre water system	1
7	granulating disc	1
8	belt conveyor	1
9	rotary shaft kiln	1
10	glass fiber dust collector	2
11	high pressure roots blower	1
12	Clinger cooler	1

13	squama board conveyor	1
14	bucket elevator	1
15	de-iron separator	1
16	cooler fan	6
17	Fuel Oil Supply	1
18	With pre-heating	1
V	cement clinker grinding section	
1	vibrating feeder	1
2	jaw crusher	1
3	bUcket elevator	1
4	automatic batching system	1
5	belt conveyor	1
6	ball mill	3
7	Dust Collector	1
8	bucket elevator	1
9	power concentrator	1
10	draughtfan	1
11	bucket elevator	1
12	hydranlic double roller crusher	2
VI	finished product package	
1	feeder	3
2	screw conveyor	1
3	bucket elevator	1
4	Rotary Screen	1
5	power concentrator	1
6	eight-nozzles Packaging machine	2
7	air compressor	2

CONTENTS

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7. Brief introduction of process procedure
8. Estimate list for project investment
9. List of main technology economy parameters

Attached: Process flow sheets

1. Production scale, production method and cement types

1.1 Production method

Dry-process production method is adopted. Rotary kiln($\Phi 3.2 \times 60\text{m}$) production line with five-stage cyclone pre-heater will be adopted.

1.2 Production scale and capacity

The production capacity is 1200t/d for clinker, while 420, 000t/a for Ordinary Portland Cement when mixed with gypsum and admixture.

1.3 Cement types

The technology and equipment adopted can produce Portland cement and Ordinary Portland cement whose strengths are 32.5MP, 42.5MP and 52.5MPa, and cement types can be adjusted according to market demand.

2. Requirements for raw materials and fuel

2.1 Calcareous material: $\text{CaO} \geq 48\%$, $\text{MgO} \leq 3\%$, $\text{K}_2\text{O} + \text{Na}_2\text{O} \leq 0.6\%$, $\text{SO}_3 \leq 1\%$

Firestone or quartz $\leq 4\%$

2.2 Argillaceous material: silica modulus $n = \text{SiO}_2 / (\text{Al}_2\text{O}_3 + \text{Fe}_2\text{O}_3) = 3.0 \sim 4.0$

Alumina modulus $p = \text{Al}_2\text{O}_3 / \text{Fe}_2\text{O}_3 = 1.5 \sim 3.5$

$\text{MgO} \leq 3\%$, $\text{SO}_3 \leq 2\%$, $\text{K}_2\text{O} + \text{Na}_2\text{O} \leq 4\%$

2.3 Other raw materials: siliceous correcting material $n > 4$

$\text{SiO}_2 = 70 \sim 90\%$ $\text{K}_2\text{O} + \text{Na}_2\text{O} \leq 4\%$

Pressure strength is better less than 1000kg/cm^2

Iron correcting material $\text{Fe}_2\text{O}_3 \geq 40\%$

Gypsum $\text{CaSO}_4 \cdot 2\text{H}_2\text{O} > 65\%$

2.4 Coal: black coal: vaporizing composition $20 \sim 35\%$, ash $\leq 28\%$

Sulfur $\leq 3\%$, low heat value $\geq 22990\text{KJ/kg}$ ($\geq 5500\text{KCal/kg}$)

2.5 Raw meal: $\text{K}_2\text{O} + \text{Na}_2\text{O} \leq 1.5\%$, $\text{CL} < 0.02\%$

Ratio of Sulfur trioxide and alkaline-earth metals oxide:

$\text{S/R} = \text{SO}_3 / (0.85\text{K}_2\text{O} + 1.29\text{Na}_2\text{O}) = 0.6 \sim 1.0$

3. Main technical characteristics

3.1 This production line adopts suspension pre-heater technology and equipment of current cement industry. With the dependable technology and equipment, great economy benefits may be acquired. New bag filter according to import technology, raw meal homogenizing silo and heat resisting exhauster adopted in this production line can improve the technology greatly.

3.2 The high-efficiency low-resistance five-stage cyclone pre-heater system with high classification efficiency, high heat

exchanging efficiency and low system resistance will be adopted at the kiln inlet, so as to increase the output of clinker. By adopting this system, apparent degree of decomposition can reach to 90-93%. In order to avoid jam in the high temperature area such as pre-heater and discharging duct, compressed air blowing device which can blow off powder automatically will be adopted at the bottom cone-shaped outlet, broadened cavity, discharging duct and transition housing of the third, fourth and fifth pre-heaters.

3.3 The following new technology will be adopted at the rotary kiln head:

- a. Multi-passage pulverized coal fuel device is adopted.
- b. The momentum flow meter regulation system is adopted for pulverized coal weighing and feeding.
- c. The high-efficiency shaft cooler will be adopted for clinker cooling.

3.4 Open-circuit raw mill and open-circuit high-fineness cement mill are adopted for grinding. This system is high in running ratio, simple in operation and small in maintenance workload.

3.5 In order to measure up to the technology requirements of the new dry process rotary kiln, control methods for electric and automation control sections should be taken like this: advanced, practicable and reliable control for main production parts, while practicable and reliable for other parts so as to realize the aim of economical and practical in control.

3.6 Great importance has been attached to the environment protection in the plan. In order to measure up to the environment protection standard, advanced and practicable dust collectors are adopted at all dust points.

4. Material balance list

No.	Name of material	Natural moisture(%)	Consumption (t/t-cl)		Material balance (t)					
			Dry	Wet	Dry			Wet		
					Hourly	Daily	Yearly	Hourly	Daily	Yearly
1	Lime stone	3	5.16	5.32	64.52	1548.0	4644000	44.32	1596	4788000
2	Clay	15	0.892	1.048	11.16	267.6	80280	13.1	314.4	94320
3	Iron powder	5	0.092	0.96	1.148	27.6	8280	1.2	28.8	8640
4	Raw meal		6.144		51.2	1843.2	552960			
5	Clinker				50	1200.0	360000			
6	Cement				58.32	1400.0	420000			
7	Admixture	20	0.516	0.644	6.452	154.8	46440	8.04	193.2	57960
8	Gypsum	5	0.188	0.200	2.36	56.4	16920	1.3	60.0	18000
9	Coal for clinkering	10	0.688	0.768	8.6	206.4	61920	9.6	230.4	69120
10	Coal for drying	10	0.068	0.76	0.852	20.4	4032	0.96	22.8	6840
11	Total coal demand				9.44	226.8	65952	10.56	253.2	75960

Remarks: 1. Annual percentage of utilization of kiln is 82.2%.

2. Raw material proportion: limestone: clay: Iron powder=84:14.5:1.5

3. Cement proportion: clinker: admixture: gypsum=85:11:4

4. Clinkering heat consumption: 3553 kJ/kgcl

5. List of Main equipment

No	Name of item	Model and specification of equipment	Power of motor (KW)	Qty (Set)	Annual running percentage rate(%)
1	Limestone crushing	PE110×850 Jaw crusher size input ≤350mm size output 40-100mm Capacity 150-225t/h	132	1	26.2
		PC-108 Hammer crusher size input ≤200mm size output ≤13mm Capacity 50-100t/h	110	1	26.2
2	Raw material grinding	Φ2.4×12m raw mill size input ≤15mm size output ≤8~10% (remainder above 4900 hole screen) Capacity 66t/h	1100	3	56.6
3	pulverized coal preparation	Φ1.7×2.5m air swept steel ball coal mill Water content of raw coal: 7-10% Outlet water content: ≤1% Fineness: ≤10~12% remainder above 4900 hole screen Capacity 2.5-3.5t/h	95	1	29.0
4	Clinker burning	Φ3.2×55m rotary kiln Five-stage cyclone pre-heater C ₁ :Φ2560 C ₂ —C ₃ :Φ2760 C ₄ —C ₅ :Φ2940 Capacity 700t/d Heat consumption: 3553KJ/Kg.Cl (850Kcal/ Kg.Cl)	110	2	82.2
5	Clinker cooling	Φ3×40m shaft cooler :1000t/d Capacity 1000t/d	90	1	82.2
6	Clinker cooling	Roots fan	150	1	82.2
7	Cement grinding	Φ2.4×10m cement mill Outlet specific surface diameter of cement: 3200cm ² /g Capacity: 60t/h	570	3	
8	Preheater Separator Heat resistant steel hang Glass fiber bag filter Multitube cooler temperature fan		290	1 1 1 1 1 1	
9	Cement packing	Fixed 2-spout packer Capacity: 30t/h		2	23.1

6. List of material storage capacity and period

Name of material	Type of storage place	Specification (m)	Qty	Storage capacity (t)	Storage period (day)
Lime stone	Pre-homogenizing silo	$\Phi 4 \times 14$	3	3000	
Clay	Shed	12×30	1	1200	
	Pre-homogenizing silo	$\Phi 4 \times 14$	2	2000	
Iron powder	Shed	12×15	1	250	
	Pre-homogenizing bin	$\Phi 4 \times 12$	2	750	
Raw meal	Round silo(silo)	$\Phi 4 \times 14$	1	1000	
Clinker	Round silo	$\Phi 4 \times 14$	2	2000	
Admixture	Round silo	$\Phi 4 \times 14$	1	1000	
Gypsum	Pre-homogenizing bin	$\Phi 4$	1	50	
Cement	Round silo	$\Phi 4 \times 14$	3	3000	
	Finished product store	24×48	1	1400	

7. Brief introduction of process procedure

7.1 Limestone crushing

The limestone block will be unloaded into hopper by mineral mountain conveyance vehicle, and crushed by PE400×600 Jaw crusher and PC-108 hammer crusher. Crushed limestone will be fed onto the pre-homogenizing limestone silos by bucket elevator.

7.2 Raw material drying, storage and blending

Clay from stockpile will be dried by $\Phi 1.5 \times 12$ m rotary dryer and fed into the 1- $\Phi 4 \times 14$ m raw material blending silo by bucket elevator. Material blending will be set as following: three $\Phi 4 \times 14$ m silo for limestone, two $\Phi 4 \times 14$ m silo for clay, and two bin for iron powder. Speed governable belt balance will be used at the bottom of material blending silo/bin. Raw meal will be blended according to the requirements and fed onto the raw mill by belt conveyor. In order to reach the optimum raw meal modulus, raw meal quality will be controlled by automatically proportioning computer system.

7.3 Raw meal grinding

Proportioned raw material will be fed onto the raw mill with size of $\Phi 2.4 \times 8$ m. Finished product ground by mill and collected by dust collector will be fed onto the raw meal homogenizing silo. Hot air for raw mill drying is supplied by hot air furnace.

7.4 Raw meal homogenizing and kiln feeding

Raw meal out of the raw mill will be fed onto the raw meal homogenizing silo (size: $\Phi 4 \times 14$ m) by bucket elevator and distributor. Homogenized raw meal will be fed onto the raw meal weighing bin by silo bottom pneumatic discharging device and bucket elevator. The raw meal weighed by speed governable belt feeder will be fed onto the pre-heater at the kiln inlet by air slide and bucket elevator.

7.5 Kiln inlet, kiln middle and kiln head

A five-stage cyclone pre-heater system will be adopted at the kiln inlet. Pre-heated raw meal will be fed into the rotary kiln ($\Phi 3.2 \times 55$ m). Pulverized coal will be sent to kiln by measuring system and multi-passage burner. Clinker out of the kiln will be cooled by $\Phi 2.5 \times 25$ m single-tube cooler, and fed onto one clinker horizontal silos (24×48 m) by bucket-chain conveyor.

7.6 Waste gas treatment of kiln inlet

Waste gas out of the pre-heater will be adjusted by $\Phi 3.85 \times 30$ m humidification tower and then sent to electric dust collector by high temperature fan. Purified gas will be discharged to the air by fan. Collected dust will be fed onto raw meal homogenizing silo.

7.7 Raw coal storage and pulverized coal preparation

Outsourced raw coal will be stored in the shed, fed into mill feeding bin by bucket elevator and belt conveyor and then fed onto air swept coal mill ($\Phi 1.7 \times 2.5$ m). Pulverized coal out of the mill will be separated by dynamic air separator. Finished product after collected by anti-explode bag filter will be fed onto pulverized coal bin. Hot air for coal drying will use kiln head waste gas. And a spare hot air furnace will be set.

7.8 Clinker and admixture storage

This section will use two round clinker silos with the size of $\Phi 4 \times 14$ m, one admixture silo with the size of $\Phi 4 \times 14$ m and one gypsum silo with the size of $\Phi 4$ m. Speed governable electrical belt balances will be used at the bottom of each silo. The clinker, gypsum and admixture will be fed onto the cement mill by belt conveyor after accurately proportioned according to the cement modulus requirement.

Outsourced gypsum block will be stored in the open stockpile, crushed by PEX250×750 fine crushing type crusher, and fed onto the $\Phi 4$ m gypsum silo by bucket elevator. Admixture from the stockpile will be fed onto

the $\Phi 4 \times 14\text{m}$ admixture silo.

7.9 Cement grinding

After material blending, clinker, admixture and gypsum will be fed into the open-circuit high-fineness cement mill (size: $\Phi 2.2 \times 11\text{m}$; capacity: 16t/h).

Product from this system has reasonable size grade and large specific surface area and it complies with fineness requirements. Finished product will be fed onto cement silos by chain conveyor and bucket elevator.

7.10 Cement storage and packing

Three silos (size: $\Phi 4 \times 14\text{m}$) will be used for cement storage. There is one silo bottom bulk loading machine. Cement from the mill will be fed onto cement silos by bucket elevator. At bottom of cement silos, screw conveyor is used to send cement to the packing system.

A fixed 2-spout packer (capacity: 60t/h) will be used for cement packing. This packer is of reliable performances. Bagged cement will be sent into the finished product store by belt conveyor to be transported outside.

8. Estimate list for project investment

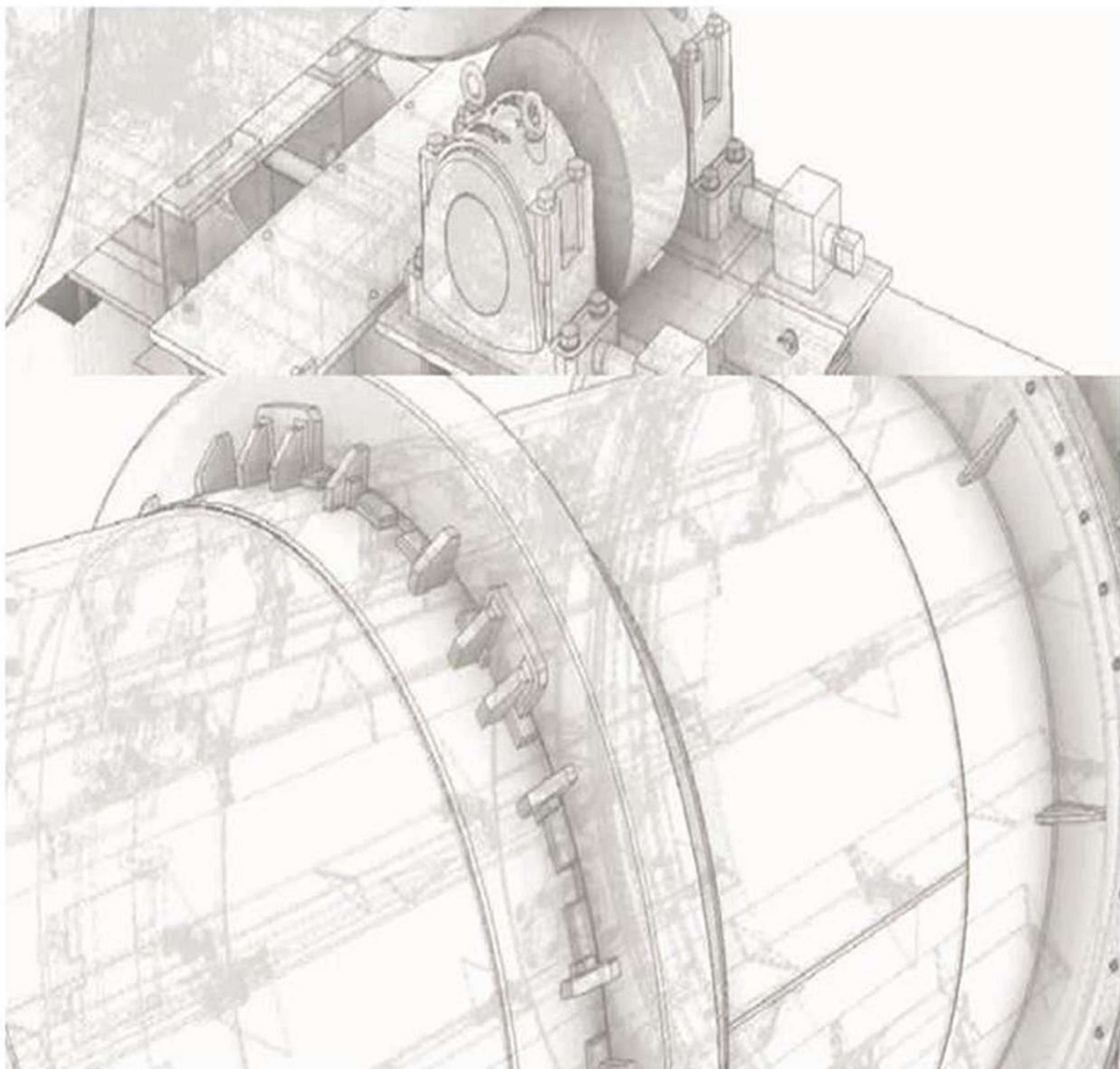
9. List of main technology economy parameters

No	Name of indexes	Unit	Quantity
1	Production scale and product types		
	Clinker	t/a	360000
	Cement	t/a	420000
2	Scale of main machine		
	Rotary kiln $\Phi 3.2 \times 55\text{m}$	set	1
	Raw mill $\Phi 2.2 \times 7.5\text{m}$	set	3
	Cement mill $\Phi 2.4 \times 8\text{m}$ Open-circuit	set	3
3	Total weight of process equipment	ton	2200
4	Installed power	KW	6000
5	Production water consumption	m^3/d	3000
6	Net production water consumption	m^3/d	900
7	Total numbers of staff	person	180
	Where: production workers	person	150
8	Labor productivity	Per ton Cement person/year	2333
9	Heat consumption of clinker burning	KJ/kg·cl	3553
10	Construction period	Mounth	14
11	Period to reach the required production capacity	mounth	6



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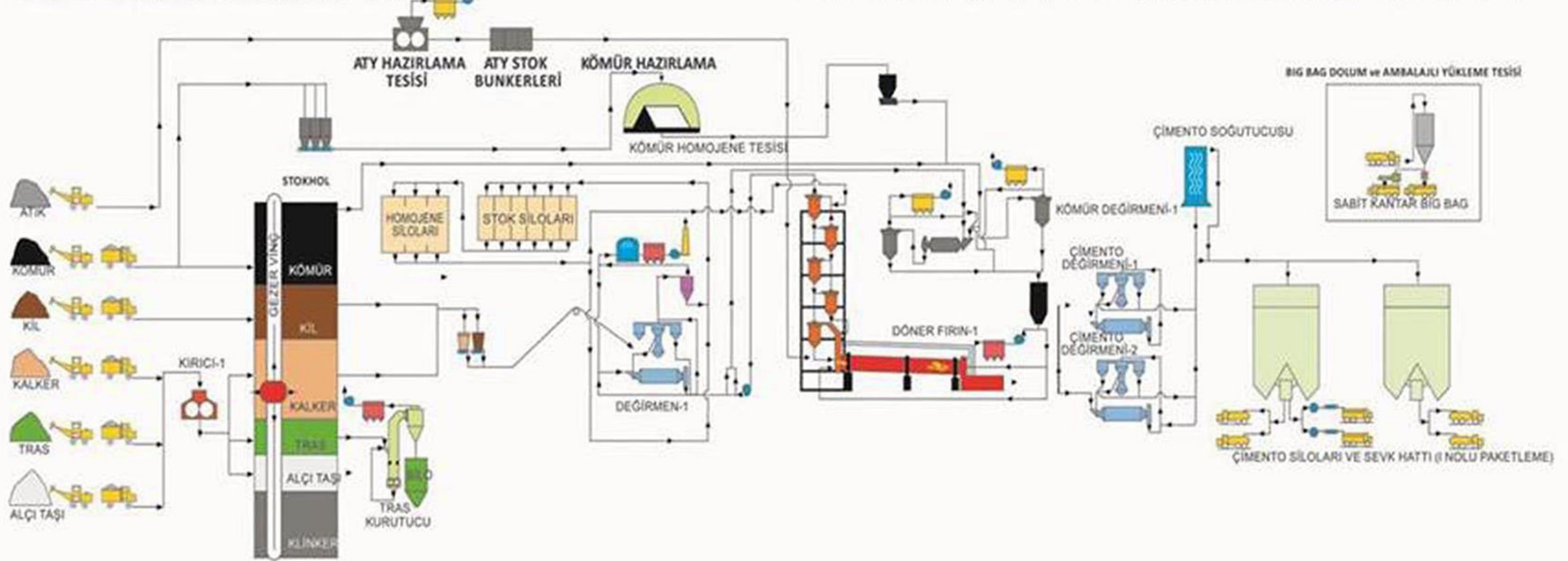
900 & 1200 TON ÇİMENTO FABRİKASI AKIŞ ŞEMASI

HAMMADDE ve YARDIMCI MADDELER FARİN HAZIRLAMA

KLİNKER HAZIRLAMA (PIŞIRME)

ÇİMENTO HAZIRLAMA (ÖĞÜTME)

AMBALAJLAMA, DOLUM VE SEVK



GEZERVİNG

GEZERVİNG-1
(2 tnepe)

KIRICI

KIRICI-1
150 t/h

KLİNKER STOK

KLİNKER STOK SİLOSU
5.00 Ton

TRAS KURUTUCU

TRAS KURUTUCU
50 t/h

DEĞİRMENİ

DEĞİRMENİ-1
50 t/h

DÖNER FIRIN

DÖNER FIRIN 1
700 t/gün

KÖMÜR DEĞİRMENİ

KÖMÜR DEĞİRMENİ-1
10 t/h

VALSİLİ PRES

VALSİLİ PRES
80 t/h

ÇİMENTO DEĞİRMENİ

ÇİMENTO DEĞİRMENİ-1
20 t/h

ÇİMENTO STOK SİLOLARI

ÇİMENTO STOK SİLOSU
3x120 Ton

AMBALAJLI - DÖKME ÇİMENTO SATIŞI

AMBALAJLI ÇİMENTO YÜKLEME
DÖNER KANTARLAR SABİT KANTAR-1
2x22.5 t/h

GEZERVİNG

GEZERVİNG-1
(2 tnepe)

KIRICI

KIRICI-1
150 t/h

KLİNKER STOK

KLİNKER STOK SİLOSU
5.00 Ton

TRAS KURUTUCU

TRAS KURUTUCU
50 t/h

DEĞİRMENİ

DEĞİRMENİ-1
50 t/h

DÖNER FIRIN

DÖNER FIRIN 1
700 t/gün

KÖMÜR DEĞİRMENİ

KÖMÜR DEĞİRMENİ-1
10 t/h

VALSİLİ PRES

VALSİLİ PRES
80 t/h

ÇİMENTO DEĞİRMENİ

ÇİMENTO DEĞİRMENİ-1
20 t/h

ÇİMENTO STOK SİLOLARI

ÇİMENTO STOK SİLOSU
3x120 Ton

GEZERVİNG

GEZERVİNG-1
(2 tnepe)

KIRICI

KIRICI-1
150 t/h

KLİNKER STOK

KLİNKER STOK SİLOSU
5.00 Ton

TRAS KURUTUCU

TRAS KURUTUCU
50 t/h

DEĞİRMENİ

DEĞİRMENİ-1
50 t/h

DÖNER FIRIN

DÖNER FIRIN 1
700 t/gün

KÖMÜR DEĞİRMENİ

KÖMÜR DEĞİRMENİ-1
10 t/h

VALSİLİ PRES

VALSİLİ PRES
80 t/h

ÇİMENTO DEĞİRMENİ

ÇİMENTO DEĞİRMENİ-1
20 t/h

ÇİMENTO STOK SİLOLARI

ÇİMENTO STOK SİLOSU
3x120 Ton

AMBALAJLI - DÖKME ÇİMENTO SATIŞI

AMBALAJLI ÇİMENTO YÜKLEME
DÖNER KANTARLAR SABİT KANTAR-1
2x22.5 t/h

GEZERVİNG

GEZERVİNG-1
(2 tnepe)

KIRICI

KIRICI-1
150 t/h

KLİNKER STOK

KLİNKER STOK SİLOSU
5.00 Ton

TRAS KURUTUCU

TRAS KURUTUCU
50 t/h

DEĞİRMENİ

DEĞİRMENİ-1
50 t/h

DÖNER FIRIN

DÖNER FIRIN 1
700 t/gün

KÖMÜR DEĞİRMENİ

KÖMÜR DEĞİRMENİ-1
10 t/h

VALSİLİ PRES

VALSİLİ PRES
80 t/h

ÇİMENTO DEĞİRMENİ

ÇİMENTO DEĞİRMENİ-1
20 t/h

ÇİMENTO STOK SİLOLARI

ÇİMENTO STOK SİLOSU
3x120 Ton



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DANIŞMANLIK**
İnş. Taah. Tur. San. Ve Dış Tic. Ltd. Şti.

Stone Crushing Konkasörü



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